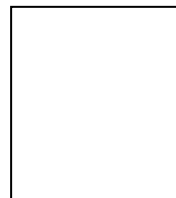


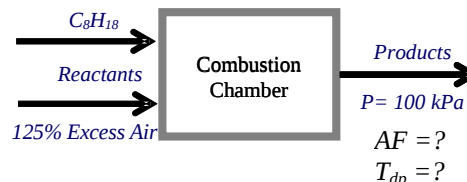
Thermodynamics II **Test #3** Saturday 29 January 2011 Time 1 hr 30 min
 Sec....เลขที่สอบ.... Name **Solution by Sommai Priprem**.....
 Examiner: Assoc.Prof.Sommai Priprem, PhD.



1) Octane (C_8H_{18}) is burned with 125 percent excess air during a combustion process. Assuming complete combustion and a total pressure of 100 kPa, determine (a) the air-fuel ratio and (b) the dew-point temperature of the products.

System: Combustion: $C_8H_{18} + 125\% \text{ ExAir}$

Assumption: SSSF, neglect ΔKE , ΔPE



Solution

Theoretical combustion equation based on 1 kmol of fuel



Combustion equation at 50% Excess Air or 150% theoretical air is



$$\begin{aligned} \text{(a)} \quad m_{\text{air}} &= (2.25 \cdot 12.5 \cdot 4.76 \cdot 28.97) &= & 3,878 \text{ kg} \\ m_{\text{fuel}} &= (8 \cdot 12) + (18 \cdot 1) &= & 114 \text{ kg} \\ \text{AF ratio} &= m_{\text{air}} / m_{\text{fuel}} &= & (3,878 \text{ kg air}) / (114 \text{ kg fuel}) \\ & &= & 34.0 \text{ kg air/kg fuel} \end{aligned}$$

Answer

(b) T_{dp} of product = T_{sat} at P_{H_2O} in product

Assume the products are ideal gases,

$$\begin{aligned} \text{therefore:} \quad P_{H_2O}/P &= n_{H_2O}/n \\ \text{Number of kmol in products, } n &= 8 + 9 + 15.6 + 105.8 \\ &= 138.38 \text{ kmol} \\ \text{kmol of } H_2O \text{ in products, } n_{H_2O} &= 9 \text{ kmol} \\ \text{Therefore; } P_{H_2O} &= (n_{H_2O}/n)P \\ &= (9/138.38)(100 \text{ kPa}) \\ &= 6.5041 \text{ kPa} \end{aligned}$$

Interporation: Table A-5

P (kPa)	T (C)
5	32.88
6.5041	37.34
7.5	40.29

ตรวจ	
รูป	1
Comb. eqn.	3
AF ratio	2
Tdp	3
สะอาด/เรียบร้อย	1

(b) the dew point temperature of the products, T_{dp} is 37.34 °C

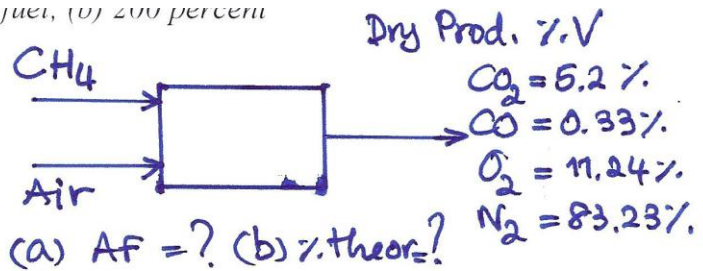
Answer

2) Methane (CH_4) is burned with dry air. The volumetric analysis of the products on a dry basis is 5.20 percent CO_2 , 0.33 percent CO , 11.24 percent O_2 , and 83.23 percent N_2 . Determine (a) the air-fuel ratio and (b) the percentage of theoretical air used.

used. Answers: (a) 34.5 kg air/kg fuel, (b) 200 percent

Solution

write combustion equation based on 100 kmol of dry products:



$$\text{N}_2 \text{ balance: } q = 83.23 / 3.76 = 22.14$$

$$\text{C balance: } p = (5.2 + 0.33) = 5.53$$

$$\text{H balance: } r = (4 \times 5.53) / 2 = 11.06$$

$$\text{check: } 0 - \text{LHS} = 2q = 44.27 \quad \text{OK}$$

$$0 - \text{RHS} = (5.2 \times 2) + (0.33) + r + 11.24 = 44.27$$

Divided by p, yields:



$$(a) \text{ AF} = \frac{(4 \times 4.76)(28.97)}{(12 + 4)} = 34.5 \text{ kg air/kg fuel} \quad \underline{\text{Ans}}$$

(b) Stoichiometric combustion equation (100% theor. air)



$$\% \text{ theor. air} = \frac{\text{AF}_{\text{actual}}}{\text{AF}_{\text{stoic}}} = \frac{n_{\text{O}_2, \text{actual}}}{n_{\text{O}_2, \text{stoic}}}$$

$$= \frac{4}{2} \times 100\% = 200\% \quad \underline{\text{Answer}}$$

Sommai
 14 January 2010

ตรวจ

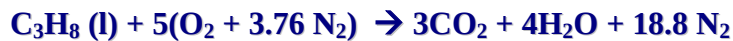
รูป 1
 Comb. eqn. 3
 AF ratio 2
 %Theor. Air 3
 สะอาด/เรียบร้อย 1

Thermodynamics II **Test #3** Saturday 29 January 2011 Time 1 hr 30 min
 Sec....เลขที่สอบ.... Name**Solution by Sommai Priprem**.....
 Examiner: Assoc.Prof.Sommai Priprem, PhD.

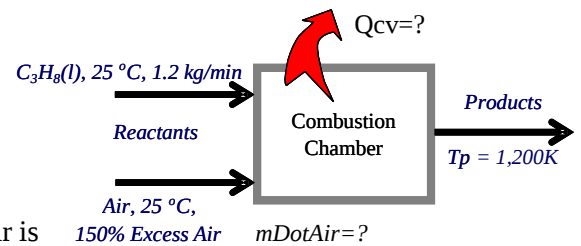
3) Liquid propane (C_3H_8) enters a combustion chamber at $25^\circ C$ at a rate of 1.5 kg/min where it is mixed and burned with 50 percent excess air that enters the combustion chamber at $25^\circ C$. If the combustion is complete and the exit temperature of the combustion gases is 1200 K, determine (a) the mass flow rate of air (in kg/min) and (b) the rate of heat transfer from the combustion chamber (in kJ/min)

Solution

Theoretical combustion equation based on 1 kmol of fuel



Combustion equation at 50% Excess Air or 150% theoretical air is



ตรวจ
 รูป 1
 Comb. eqn. 2
 AF ratio 1
 Qdot 5
 สะอาด/เรียบร้อย 1

(a)	m_{air}	=	$(7.5 \times 4.76 \times 28.97)$	=	1,034.2	kg
	m_{fuel}	=	$(3 \times 12) + (8 \times 1)$	=	44	kg
	AF ratio	=	m_{air} / m_{fuel}	=	$(1,034.2 \text{ kg air}) / (44 \text{ kg fuel})$	
				=	23.51	kg air/kg fuel
	$m_{dot, air}$	=	$m_{dot, fuel} \text{ AF}$	=	$(1.5 \text{ kg/min})(23.51 \text{ kg air/kg fuel})$	
				=	35.3 kg air/min	Answer

(b) 1st Law: cv. Combustion Chamber, SSSF, neglect Wcv, ΔKE , ΔPE

$$Q_{cv} + H_R = H_P$$

because T_R at 25 C then all $\Delta h_i = 0$ then $H_R = \sum_R n_i (\bar{h}_f + \Delta \bar{h})_i = \bar{h}_{f, C_3H_8(l)}$

$$H_P = \sum_P n_e (\bar{h}_f + \Delta \bar{h})_e$$

Table A-26 enthalpy of formation of $C_3H_8(g)$, $\bar{h}_{f, C_3H_8(g)}^\circ = -103,850$ kJ/kmol

Table A-26 enthalpy of vaporization of C_3H_8 , $\bar{h}_{fg, C_3H_8} = 15,060$ kJ/kmol

$$H_R = \bar{h}_{f, C_3H_8(l)}^\circ = \bar{h}_{f, C_3H_8(g)}^\circ - \bar{h}_{fg, C_3H_8} = -118,910 \text{ kJ/kmol}$$

Calculation for H_R : Products: at 1200 K

Components	n	$\bar{h}_f^\circ$	$\bar{h}_{1200}$	$\bar{h}_{298}$	$\bar{h}_T - \bar{h}_{298}$	$n_e (\bar{h}_f + \Delta \bar{h})_e$
CO2	3.0	-393,520	53,848	9,364	44,484	-1,047,108
H2O	4.0	-241,820	44,380	9,904	34,476	-829,376
O2	2.5	-	38,447	8,682	29,765	74,413
N2	28.2	-	36,777	8,669	28,108	792,646
$H_P = \sum_P n_e (\bar{h}_f + \Delta \bar{h})_e$						-1,009,426

$$Q_{cv} = H_P - H_R = [(-1,009,426) - (-118,910)] \text{ kJ/kmol fuel}$$

$$= -890,516 \text{ kJ/kmol fuel}$$

$$Q_{dot} = m_{fuel} (Q_{cv}/M) = (1.5 \text{ kg/min})(-890,516 \text{ kJ/kmol fuel}/44 \text{ kg/kmol})$$

the rate of heat transfer from the combustion chamber, **Qdot is 30,358 kJ/min**

Answer