

ภาควิชาวิศวกรรมเครื่องกล

คณะวิศวกรรมศาสตร์ มหาวิทยาลัยขอนแก่น

ข้อสอบกลางภาค ประจำภาคต้น ปีการศึกษา 2553

วิชา **185 231 Thermodynamics I**

วันที่ 6 สิงหาคม 2553

เวลา 13.00 — 16.00 น.

ผู้ออกและตรวจข้อสอบ: รศ.ดร.สมหมาย ปรีเปรม ผศ.ดร.ปริมพัฒน์ สุจ้านงโตกุล อ.ดร.อักรพล จันทรอ่อน

คำสั่ง

1. ให้เขียน ชื่อ-สกุล กลุ่ม และที่นั่งสอบ ลงในกระดาษข้อสอบทุกแผ่น
2. ข้อสอบทั้งหมดมี 5 ข้อ จำนวน 8 แผ่นรวมทั้งแผ่นนี้ ให้ทำทุกข้อ
3. มีตาราง Thermodynamics ให้
4. อนุญาตให้ใช้เครื่องคำนวณที่ไม่มีการบันทึกข้อมูลของรายวิชานี้ไว้
5. ห้ามนำเอกสารใดๆออกจากห้องสอบ
6. ให้ทำข้อสอบในแผ่นข้อสอบของข้อนั้นๆเท่านั้น (สามารถใช้ด้านหลังได้)

ชื่อ-สกุล.....รหัส..... Section.....ที่นั่งสอบ.....

ข้อ	คะแนนเต็ม	คะแนน
1	10	
2	10	
3	10	
4	10	
5	10	
รวม	50	

ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

1) Choose the correct answer and fill X into the answer sheet

Answer sheet for problem 1

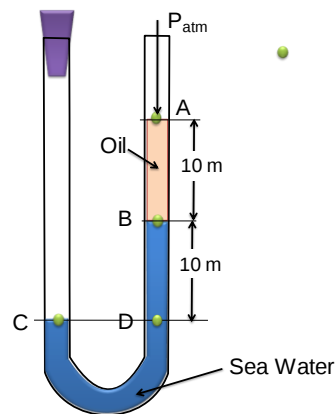
No.	a	b	c	d	e	f
1.1			X			
1.2				X		
1.3					X	
1.4			X			
1.5						X
1.6	X					
1.7						X
1.8		X				
1.9				X		
1.10			X			

1.10 ตอบ 2,755.3 kJ/kg ข้อ c เป็นคำตอบที่ใกล้เคียงที่สุด

1.1) Find the absolute pressure of point C.

Let $P_{\text{atm}} = 1 \text{ bar}$, oil density 800 kg/m^3
and density of sea water = 1300 kg/m^3

- a) 118 kPa
- b) 206 kPa
- c) 306 kPa
- d) 418 kPa
- e) 518 kPa
- f) 506 kPa

1.2) Water at 2 MPa (absolute) and 80°C , the density of the water is

- a) 0.001 kg/m^3
- b) 0.002 kg/m^3
- c) 877.3 kg/m^3
- d) 971.8 kg/m^3
- e) 786.7 kg/m^3
- f) 455.5 kg/m^3

ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

- 1.3) Saturated liquid water 5 kg 200 kPa gage pressure is heated to be saturated steam at constant pressure process. If the atmospheric pressure is 0.1 MPa, the amount of heat transfer to the water is
- a) 200.2 kJ/kg
 - b) 400 kJ/kg
 - c) 216.38 kJ
 - d) 5.00 kJ
 - e) 10.819 MJ
 - f) 2163.8 kJ
- 1.4) Saturated liquid-vapor mixture of 5 kg water at $P = 0.2$ MPa (absolute) with quality $x = 1.0$ is condensed until the quality becomes $x = 0.4$. The amount of condensate (liquid) change is
- a) 1.0 kg
 - b) 2.0 kg
 - c) 3.0 kg
 - d) 4.0 kg
 - e) 5.0 kg
 - f) 0.5 kg
- 1.5) Air at $P_1 = 1$ MPa absolute and 200°C is contained in a closed airtight rigid chamber. The whole system is cooled till the temperature drops to 40°C . The final air pressure in the chamber is
- a) 1.23 kPa
 - b) 22.6 kPa
 - c) 123.8 kPa
 - d) 287.0 kPa
 - e) 466.7 kPa
 - f) 661.7 kPa
- 1.6) For gas A, the value of gas constant is $300\text{ J/kg}\cdot\text{K}$ while the C_V is $800\text{ J/kg}\cdot\text{K}$. If the gas receives heat that make the temperature increases by 40°C . Find the change of the specific enthalpy of the gas.
- a) 44.0 kJ/kg
 - b) 33.0 kJ/kg
 - c) 22.0 kJ/kg
 - d) 11.0 kJ/kg
 - e) 5.0 kJ/kg
 - f) 2.52 kJ/kg

ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

- 1.7) The refrigerant-12 at the temperature of 4°C and $x = 0.3$ enters evaporator and leaves with the pressure at 0.32 MPa and 30°C . The change of specific enthalpy is
- a) 149.47 kJ/kg
 - b) 39.76 kJ/kg
 - c) 189.23 kJ/kg
 - d) 77.81 kJ/kg
 - e) 67.78 kJ/kg
 - f) No correct answer
- 1.8) To estimate the property (y) of compressed liquid at given pressure and temperature. We estimate the property by using
- a) $y = y_{g@T}$
 - b) $y = y_{f@T}$
 - c) $y = y_{f@P}$
 - d) $y = y_{g@P}$
 - e) $y = y_{fg@T}$
 - f) $y = y_{fg@P}$
- 1.9) We can assume that the pressure of the air is uniform in the storage tank because
- a) the air is clear in color
 - b) air density is very high
 - c) air density is high
 - d) air density is light
 - e) the earth is large
 - f) the tank is closed
- 1.10) Superheated steam at 0.2 MPa absolute and 270°C , the value of specific internal energy is
- a) 2971.00 kJ/kg
 - b) 3071.80 kJ/kg
 - c) 2731.20 kJ/kg
 - d) 2808.60 kJ/kg
 - e) 2200.78 kJ/kg
 - f) 3011.32 kJ/kg
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ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

2. An ideal gas is heated in a piston-cylinder device. During the process, the pressure changes from 100 kPa to 800 kPa according to the relation $P = aV + b$, where $a = 1,220$ kPa/m³ and b is a constant. The final volume of the gas is 0.7738 m³. Then the gas is heated further but this time the volume is kept constant to the final pressure of 1,200 kPa.

- Draw a P-V diagram shows the process occurred.
- Calculate the work done by the system in kJ using integration method.

Solution:

a) P-V diagram

b) Work done

$$P = aV + b$$

$$P_2 = aV_2 + b$$

$$800 = (1220 \times 0.7738) + b$$

$$b = 800 - (1220 \times 0.7738) = -144$$

$$V_1 = \frac{P_1 - b}{a} = \frac{100 - (-144)}{1220} = 0.2 \text{ m}^3$$

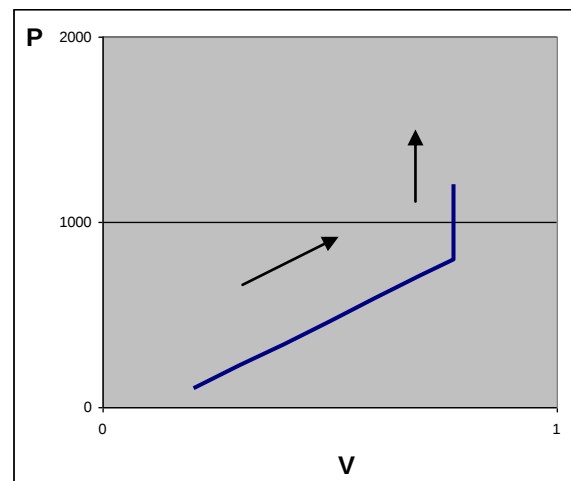
$$W = \int_{V_1}^{V_2} (aV + b) dV$$

$$W = \frac{a}{2} V^2 + bV \Big|_{V_1}^{V_2}$$

$$W = \frac{a}{2} (V_2^2 - V_1^2) + b(V_2 - V_1)$$

$$W = \left(\frac{1220}{2} (0.7738^2 - 0.2^2) - 144 \times (0.7738 - 0.2) \right)$$

$$W = 258.22 \text{ kJ}$$

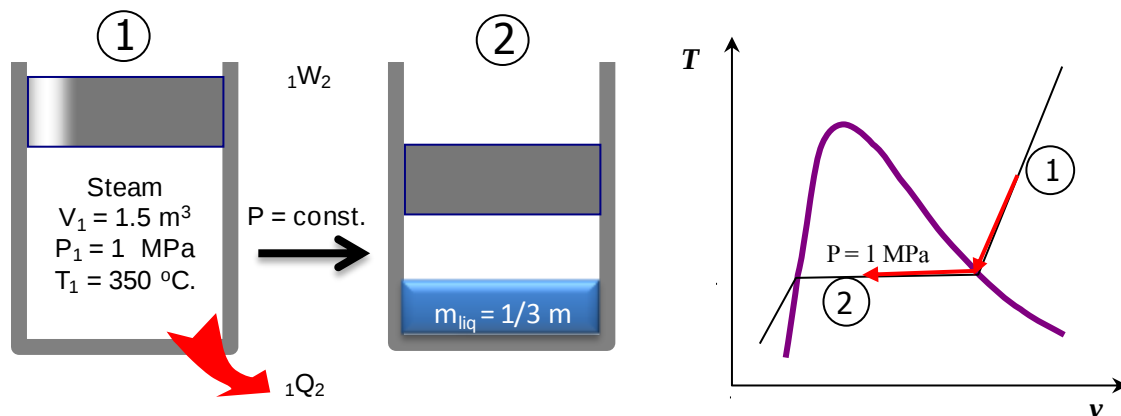


ชื่อ-สกุล..... *Sommai Priprem*..... รหัส..... กลุ่ม..... ที่นั่งสอบ.....

3. A piston-cylinder device contains steam initially at 1 MPa, 350°C, and 1.5 m³. Steam is allowed to cool at constant pressure until one-third of the mass of the steam condensed. Show the process on a T-v diagram with respect to saturation lines (1 mark) and determine,

- the mass of the steam (1 marks)
- the quality (x) at the final state, (1 mark)
- the amount of work during the process, (3 marks)
- the amount of heat transfer. (3 marks)

(การทำงานอย่างเป็นลำดับขั้นตอนที่ดี การเขียนอย่างเรียบร้อยดูง่ายและสะอาด 1 คะแนน)



System Water in the Piston-Cylinder: Closed System: $P = \text{const}$

Assumption Neglect change in KE, PE

Analysis

$$m = V_1/v_1$$

$$-{}_1Q_2 \text{ until } \frac{1}{2} m \text{ condensed} \rightarrow \text{mixture: } x_2 = m_{\text{vap}}/m$$

$${}_1W_2 = mP_1(v_2 - v_1)$$

$${}_1Q_2 = U_2 - U_1 + {}_1W_2$$

Solution

(a) Find mass of the steam:

State 1 $P_1 = 1 \text{ MPa}$, $T_1 = 350^\circ\text{C}$, Table A-5 $T_1 > T_{\text{sat}} \rightarrow$ Superheated vapor

Table A-6 $v_1 = 0.2825 \text{ m}^3/\text{kg}$; $u_1 = 2,875.2 \text{ kJ/kg}$

$$V_1 = 1.5 \text{ m}^3$$

$$m = V_1/v_1 = (1.5 \text{ m}^3)/(0.2825 \text{ m}^3/\text{kg})$$

the mass of steam is 5.31 kg Answer

(b) Find the steam quality

State 2 $P_2 = P_1 = 1 \text{ MPa}$ and $1/3m$ condensed $\rightarrow m_{\text{vap}} = 1/3m$

therefore; quality, $x = m_{\text{vap}}/m = 2/3 = 0.6667$ Answer

(c) Find Work : Boundary work: Process $P = c$; ${}_1W_2 = mP_1(v_2 - v_1)$

Table A-5 $v_f = 0.001127 \text{ m}^3/\text{kg}$; $v_g = 0.19444 \text{ m}^3/\text{kg}$

$$v_2 = v_f + xv_g = (0.001127 + 0.6667 \times 0.19444) = 0.1300 \text{ m}^3/\text{kg}$$

$${}_1W_2 = (5.31 \text{ kg})(1000 \text{ kPa})(0.1300 - 0.2825) \text{ m}^3/\text{kg} = -809.7 \text{ kJ}$$

The work done on the system during the process is **809.7 kJ** Answer

(d) Find Heat

1st Law: ${}_1Q_2 = m(u_2 - u_1) + {}_1W_2$

Table A-5 at 1 MPa $u_f = 761.68 \text{ kJ/kg}$; $u_{fg} = 1,822.0 \text{ kJ/kg}$

$$u_2 = u_f + xu_{fg} = (761.88 + 0.6667 \times 1,822.0) = 1,976.3 \text{ kJ/kg}$$

$$m(u_2 - u_1) = (5.31 \text{ kg})(1,976.3 - 2,875.2) \text{ kJ/kg} = -4,772.7 \text{ kJ}$$

then, ${}_1Q_2 = (-4,772.7 \text{ kJ}) + (-809.7 \text{ kJ}) = -5,582.4 \text{ kJ}$

The amount of heat transfer out of the steam is **5,582.4 kJ** Answer *Sommai Priprem*

ชื่อ-สกุล..... 1202 804 รหัส กลุ่ม..... ที่นั่งสอบ.....

4. A steam turbine operates with 2 MPa absolute pressure and 400 °C at the inlet. The steam exits the turbine at 40 °C and $x = 0.9$. The mass flow rate of the steam is 16 kg/s. The turbine produces mechanical power by 1.1 MW. Neglect the kinetic and potential energies,

- write the energy balance equation of this turbine process,
- determine the total enthalpy change in kW,
- calculate the rate of heat loss from the turbine in kW.

Solution.

Assumption. S-S-S-F.

state ①; superheated steam.

$$h_1 = 3247.6 \text{ kJ/kg}$$

state ②; sat. mixture. (40°C)

$$h_f = 167.57 \frac{\text{kJ}}{\text{kg}}; h_{fg} = 2406.7 \frac{\text{kJ}}{\text{kg}}$$

$$\therefore h_2 = h_f + x h_{fg} = 167.57 + (0.9)(2406.7) = 2333.6 \text{ kJ/kg}$$

a) Energy Balance

$$\dot{Q} - \dot{W} = \Delta H + \cancel{\Delta KE} + \cancel{\Delta PE} \quad \text{--- ①}$$

Marks.

2

$$\begin{aligned} \text{b) } \Delta H &= \dot{m} (h_2 - h_1) = 16 (2333.6 - 3247.6) \frac{\text{kg}}{\text{s}} \cdot \frac{\text{kJ}}{\text{kg}} \\ &= -14,624 \text{ kW} \end{aligned}$$

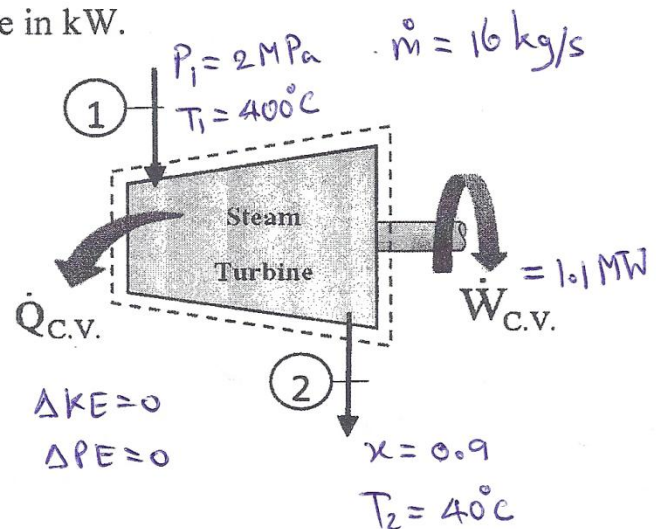
4 Marks

e) From Energy Balance;

$$\dot{Q} - (+1100) = -14624$$

$$\dot{Q} = -13524 \text{ kW}$$

4 Marks



ชื่อ-สกุล..... *Sommai Priprem*.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

5. Refrigerant-12 enters the evaporator of an air conditioner at 200 kPa with a quality of 25% at a rate of 2.1 kg/min and leaves as saturated vapor at the same pressure. Air enters at 100 kPa and 28°C. It is required that the air leaves the evaporator at 16°C at 100 kPa. Assume air as an ideal gas and use constant specific heat at 300 K in the calculation. State any assumption made(1 marks). Determine

(a) the mass flow rate of the air (in kg/min) and, (6 marks)

(b) the volume flow rate of the air at inlet (in m³/min). (3 marks)

(การทำงานอย่างเป็นลำดับขั้นตอนที่ดี การเขียนอย่างเรียบร้อยดูง่ายและสะอาด เป็นองค์ประกอบในการพิจารณาให้คะแนนด้วย)

System: CV The evaporator : R-12 and Air
Assumption: SSSF process;

$\dot{Q}_{cv} = 0$; $\dot{W}_{cv} = 0$
and neglect ΔKE and ΔPE

Solution:

1st Law:

$$\dot{Q}_{cv} + \sum \dot{m}_i h_i = \dot{W}_{cv} + \sum \dot{m}_e h_e$$

$$[\dot{m}_1 h_1 + \dot{m}_3 h_3] = [\dot{m}_2 h_2 + \dot{m}_4 h_4]$$

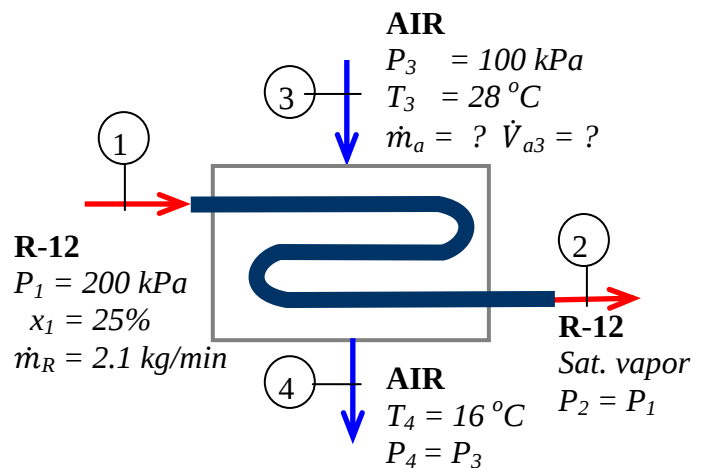
$$\dot{m}_1 = \dot{m}_2 = \dot{m}_r; \dot{m}_3 = \dot{m}_4 = \dot{m}_a$$

$$\dot{m}_a (h_3 - h_4) = \dot{m}_r (h_2 - h_1)$$

$$\dot{m}_a C_{pa} (T_3 - T_4) = \dot{m}_r (h_2 - h_1)$$

$$\dot{m}_a = \frac{\dot{m}_r (h_2 - h_1)}{C_{pa} (T_3 - T_4)} \quad (1)$$

$$\dot{V}_3 = \dot{m}_a v_3; \quad v_3 = \frac{R_a T_3}{P_3} \quad (2)$$



R-12-side data and calculations			
State 1 mixture			
P_1	=	200	kPa
x_1	=	25%	
$\dot{m}_r$	=	2.1	kg/min
From Table A-12 at 200 kPa			
h_f	=	24.57	kJ/kg
h_{fg}	=	157.5	kJ/kg
h_1	=	63.945	kJ/kg
State 2 Saturated vapor: Table A-12			
P_2	=	140	kPa
$h_2 = h_g$	=	182.07	kJ/kg
$\dot{m}_r (h_2 - h_1)$	=	248.06	kJ/min

Air-side data and calculations			
State 3 and 4 Ideal gas			
P_3	=	100	kPa
T_3	=	28	C
T_4	=	16	C
From table A-2 at 300K			
C_p	=	1.005	kJ/kgK
$C_p (T_3 - T_4)$	=	12.06	kJ/kg
Substitute in equation (1) and (2)			
$\dot{m}_a$	=	20.57	kg/min
R	=	0.287	kJ/kgK
$v_3 = RT/P$	=	0.86387	m ³ /kg
$\dot{V}_{dot} = \dot{m} v$	=	17.77	m³/min

Answer

Answer