

ภาควิชาวิศวกรรมเครื่องกล

คณะวิศวกรรมศาสตร์ มหาวิทยาลัยขอนแก่น

ข้อสอบปลายภาค ประจำภาคต้น ปีการศึกษา 2554

วิชา **185 231 Thermodynamics I**

วันที่ วันพุธที่ 28 กันยายน 2554

เวลา 08.30 — 11.30 น.

ผู้ออกและตรวจข้อสอบ: รศ.ดร.สมหมาย ปรีเปรม ผศ.ดร.ปริมพัฒน์ สุจ้านงโตกุล อ.ดร.อักรพล จันทรอ่อน

คำสั่ง

1. ให้เขียน ชื่อ-สกุล กลุ่ม และที่นั่งสอบ ลงในกระดาษข้อสอบทุกแผ่น
2. ข้อสอบทั้งหมดมี 5 ข้อ ให้ทำทุกข้อ
3. มีตาราง **Thermodynamics** ให้
4. อนุญาตให้ใช้เครื่องคำนวณที่ไม่มีการบันทึกข้อมูลของรายวิชานี้ไว้
5. ห้ามนำเอกสารใดๆออกจากห้องสอบ
6. ให้ทำข้อสอบในแผ่นข้อสอบของข้อนั้นๆเท่านั้น (สามารถใช้ด้านหลังได้)

ชื่อ-สกุล.....รหัส..... **Section**.....ที่นั่งสอบ.....

ข้อ	คะแนนเต็ม	คะแนน
1	10	
2	10	
3	10	
4	10	
5	10	
รวม	50	

ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

2. An air standard Otto cycle has a compression ratio of 9.0. The state of air at the beginning of the compression process is 80 kPa and 30°C. The heat input during the heat addition process is 1,000 kJ/kg. Calculates by using constant specific heats at 900K, determine

- (a) Write the name of the 4 processes (1 mark)
 (b) draw the P-v and T-s diagram, (1 mark)
 (c) the amount of heat rejected per cycle, (3 mark)
 (d) the net work per cycle, (1 mark)
 (e) the thermal efficiency and (1 mark)
 (f) the mean effective pressure. (2 mark)
 การทำงานที่เป็นระบบ เรียบร้อยและสะอาด (1 mark)

Process	Process name	P-v diagram	T-s diagram
1-2	<i>Isentropic Compression</i>		
2-3	Constant Volume Heat Addition		
3-4	Isentropic Expansion		
4-1	Constant Volume Heat Rejection		

Solution

Assumption: Air Standard Otto cycle, constant sp.ht.at 900K

Given: $P_1 = 80 \text{ kPa}$, $T_1 = 30^\circ\text{C}$, $r_v = 9$; $q_H = 1,000 \text{ kJ/kg}$

Constants: Table A-1: $R = 0.287 \text{ kJ/kgK}$;

Table A-2(b): $C_v = 0.834 \text{ kJ/kgK}$, $k = 1.344$

therefore: $k-1 = 0.344$; $r_v^{(k-1)} = 2.1294$ and $r_v^k = 19.1647$

To determine Temperature at each state point:

Process 1-2 Isentropic Expansion of ideal gas:

$Pv^k = \text{const.}$ and $Tv^{k-1} = \text{const.}$ **therefore**

$$T_2 v_2^{(k-1)} = T_1 v_1^{(k-1)}$$

$$\begin{aligned} T_2 &= T_1 (v_1/v_2)^{(k-1)} = T_1 r_v^{(k-1)} \\ &= (303\text{K})(9.0)^{0.344} = \mathbf{645.2 \text{ K}} \end{aligned}$$

Process 2-3 Constant Volume Heat Addition: ($+q_H = 1,000 \text{ kJ/kg}$)

Apply 1st law for a closed system

$${}_2q_3 = {}_2w_3 + (u_3 - u_2) \quad \text{where } {}_2w_3 = 0 \text{ because } v = \text{constant}$$

$$\text{Therefore, } q_H = {}_2q_3 = u_3 - u_2 = C_v(T_3 - T_2)$$

$$\begin{aligned} T_3 &= T_2 + {}_2q_3/C_v \\ &= (645.2\text{K}) + (1,000\text{kJ/kg}) / (0.834\text{kJ/kgK}) = \mathbf{1,844.3 \text{ K}} \end{aligned}$$

Process 3-4 Isentropic Expansion of ideal gas: $Pv^k = \text{const.}$ and $Tv^{k-1} = \text{const.}$

$$T_4 = T_3 / r_v^{(k-1)} = (1,844.3 \text{ K}) / (9.0)^{0.344} = \mathbf{866.1 \text{ K}}$$

Process 4-1 Constant Volume Heat Rejection**Apply 1st law for a closed system**

$${}_4q_1 = {}_1w_4 + (u_1 - u_4) \quad \text{where } {}_1w_4 = 0 \text{ because } v = \text{constant}$$

$$\text{Therefore, } {}_4q_1 = C_v(T_1 - T_4) = (0.834 \text{ kJ/kgK})(303 - 866.1) \text{ K} = -469.6 \text{ kJ/kg}$$

(c) The amount of heat rejected per cycle, $q_L = |{}_4q_1| = 469.6 \text{ kJ/kg}$ Answer

(d) To determine the net work per cycle, apply 1st law for a cycle

$$w_{\text{net}} = q_{\text{net}}$$

$$\text{The net work per cycle, } w_{\text{net}} = q_H - q_L$$

$$= (1,000 - 469.6) \text{ kJ/kg} = 530.4 \text{ kJ/kg} \quad \text{Answer}$$

$$\text{(e) The Thermal Efficiency, } \eta_{\text{th}} = w_{\text{net}}/q_H * 100\%$$

$$= (530.4 \text{ kJ/kg}) / (1,000 \text{ kJ/kg}) * 100$$

$$= 53.04 \% \quad \text{Answer}$$

$$\text{(f) Mean effective pressure, } \text{MEP} = W_{\text{net}} / (v_1 - v_2)$$

$$\begin{aligned} \text{State 1: ideal gas equation: } v_1 &= RT_1/P_1 = (0.287 \text{ kJ/kgK})(303 \text{ K}) / (80 \text{ kPa}) \\ &= 1.08701 \text{ m}^3/\text{kg} \end{aligned}$$

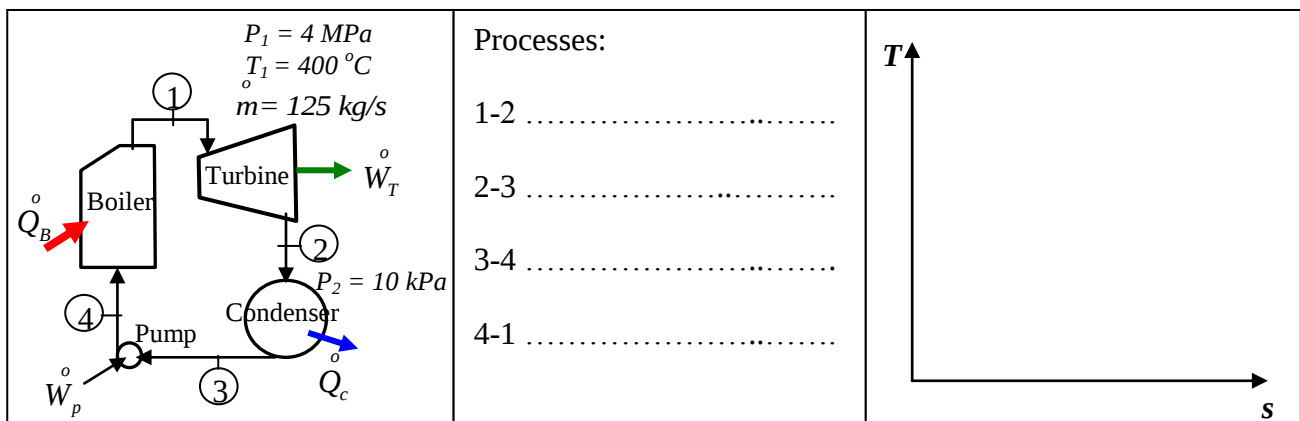
$$\text{therefore, } v_2 = v_1/r_v = 0.12078 \text{ m}^3/\text{kg}$$

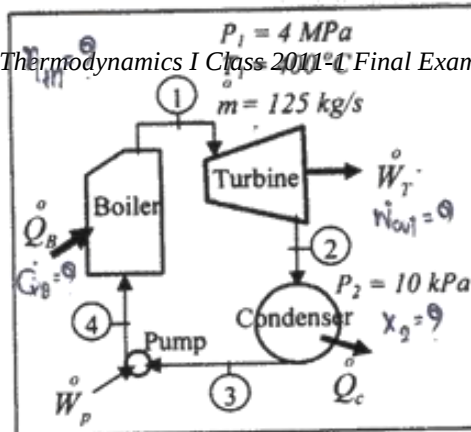
$$\text{MEP} = (530.4 \text{ kJ/kg}) / (1.08701 - 0.12078) \text{ m}^3/\text{kg} = 548.9 \text{ kPa}$$

$$\text{The Mean Effective Pressure of the cycle, MEP is } 548.9 \text{ kPa} \quad \text{Answer}$$

ชื่อ-สกุล.....รหัส.....กลุ่ม.....ที่นั่งสอบ.....

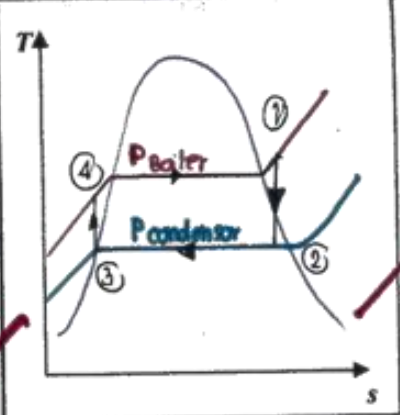
4) Consider a steam power plant which operates on a simple **ideal Rankine cycle**, as the figure shown below. Steam enters the turbine at 4 MPa and 400°C with a mass flow rate of 125 kg/s. After that it is cooled in the condenser at a pressure of 10 kPa. **In the given block, write the 4-processes and show the cycle on a T-s diagram with respect to saturation lines, state any assumption made, and determine (a) the quality of the steam at the turbine exit, (b) the net power output of the power plant in MW, (c) the rate of heat input to the boiler in MW, and (d) the thermal efficiency of the cycle. (10 Marks)**





Processes:

- 1-2 Isentropic expansion
- 2-3 $-Q_C$, $P = \text{constant}$
- 3-4 Isentropic compression
- 4-1 $+Q_H$, $P = \text{constant}$



System: Ideal Rankine cycle.

a) the quality of the steam at turbine exit.

Analysis: process 1-2 Isen. expan. + W_T C.V. Turbine; 1st law; Open System; SSF ✓

$$\dot{Q} + h_1 = \dot{W}_T + h_2$$

$$\dot{W}_T = h_1 - h_2 \rightarrow \text{①}$$

state ① saturated vapor: Table A-5

Table A-5 @ $P_1 = 4 \text{ MPa}$ and $T_1 = 400^\circ\text{C}$ $T_1 > T_{\text{sat}} \Rightarrow$ Super heatTable A-6 @ $P_1 = 4 \text{ MPa}$ and $T_1 = 400^\circ\text{C}$ on h_1

$$h_1 = h @ P_1 = 4 \text{ MPa} = 3213.6 \text{ kJ/kg}$$

$$S_1 = S @ P_1 = 4 \text{ MPa} = 6.7690 \text{ kJ/kg}\cdot\text{K}$$

state ② saturated vapor @ $P_2 = 10 \text{ kPa}$ and $S_1 = S_2 = 6.7690 \text{ kJ/kg}\cdot\text{K}$ Table A-5 $S_f < S_2 < S_g \Rightarrow$ mixture

$$h_2 = h_f + x_2 h_{fg} \rightarrow \text{②}$$

$$\begin{aligned} \text{on } x_2 \text{ on } \text{Table A-5} \\ S_2 = S_f + x_2 S_{fg} \quad \left. \begin{aligned} h_f &= 191.83 \text{ kJ/kg} \\ h_{fg} &= 2392.8 \text{ kJ/kg} \\ S_f &= 0.6493 \text{ kJ/kg}\cdot\text{K} \\ S_{fg} &= 7.5009 \text{ kJ/kg}\cdot\text{K} \end{aligned} \right\} \\ x_2 = \frac{S_2 - S_f}{S_{fg}} = \frac{6.7690 - 0.6493}{7.5009} = 0.816 \end{aligned}$$

$$x_2 = \frac{6.7690 - 0.6493}{7.5009} \text{ kJ/kg}\cdot\text{K}$$

$$x_2 = 0.816$$

Ans. the quality of the steam at turbine exit (x_2) = 0.816

b) the net power output of the power plant

Analysis: on ① $h_1 = 3213.6$

$$h_2 = 191.83 \text{ kJ/kg} + (0.816)(2392.8 \text{ kJ/kg})$$

$$h_2 = 2144.355 \text{ kJ/kg}$$

$$\text{on ① } \dot{W}_T = (3213.6 - 2144.355) \text{ kJ/kg}$$

$$\dot{W}_T = 1069.245 \text{ kJ/kg}$$

$$\dot{W}_{\text{out}} = \dot{m}(\dot{W}_T) = (125 \text{ kg/s})(1069.245 \text{ kJ/kg})$$

$$\dot{W}_{\text{out}} = 133.66 \text{ MW}$$

Ans. the net power output ($\dot{W}_{\text{out}}$) = 133.66 MW ✓

c) the rate of heat input to the boiler

Analysis: process ④-① $+Q_H$, $P = \text{constant}$; C.V. Boiler

$$\dot{Q}_H + h_4 = \dot{W}_P + h_1$$

$$\dot{Q}_H = h_1 - h_4 \rightarrow \text{③}$$

process ③-④ Isentropic compression

C.V. Pump; 1st law; Open System; SSF

$$\dot{Q} + h_3 = \dot{W}_P + h_4$$

$$\dot{W}_P = h_4 - h_3 \rightarrow \text{④}$$

state ③ Sat. liquid Table A-5

$$h_3 = h_f @ P_3 = 10 \text{ kPa} = 191.83 \text{ kJ/kg}$$

$$v_3 = v_f @ P_3 = 10 \text{ kPa} = 0.00101 \text{ m}^3/\text{kg}$$

on ④ fluid $\Rightarrow$ liquid $v_3 = v = \text{constant}$

$$\dot{W}_P = v_3 (P_4 - P_3)$$

$$\dot{W}_P = (0.00101 \text{ m}^3/\text{kg})(10 - 4000) \text{ kPa}$$

$$\dot{W}_P = -4.03 \text{ kJ/kg} = 4.03 \text{ kJ/kg}$$

on ④ on h_4

$$-4.03 \text{ kJ/kg} = 191.83 \text{ kJ/kg} - h_4$$

$$h_4 = 195.86 \text{ kJ/kg}$$

$$\text{on ③ } \dot{Q}_H = (3213.6 - 195.86) \text{ kJ/kg} = 3017.74 \text{ kJ/kg}$$

$$\dot{Q}_H = \dot{m} \dot{Q}_H = (125 \text{ kg/s})(3017.74 \text{ kJ/kg}) = 377.22 \text{ MW}$$

Ans. the rate of heat input to the boiler ($\dot{Q}_H$) = 377.22 MW ✓

d) the thermal efficiency of cycle

$$\text{Analysis: } \eta_{\text{th}} = \frac{\dot{W}_{\text{net}}}{\dot{Q}_H} \rightarrow \text{⑤}$$

$$\dot{W}_{\text{net}} = \dot{W}_T - \dot{W}_P = (1069.245 - 4.03) \text{ kJ/kg}$$

$$\dot{W}_{\text{net}} = 1065.215 \text{ kJ/kg}$$

$$\text{on ⑤ } \eta_{\text{th}} = \frac{1065.215 \text{ kJ/kg}}{3017.74 \text{ kJ/kg}} \times 100\%$$

$$= 35.3\%$$

Ans. the thermal efficiency (η_{th}) = 35.3% ✓