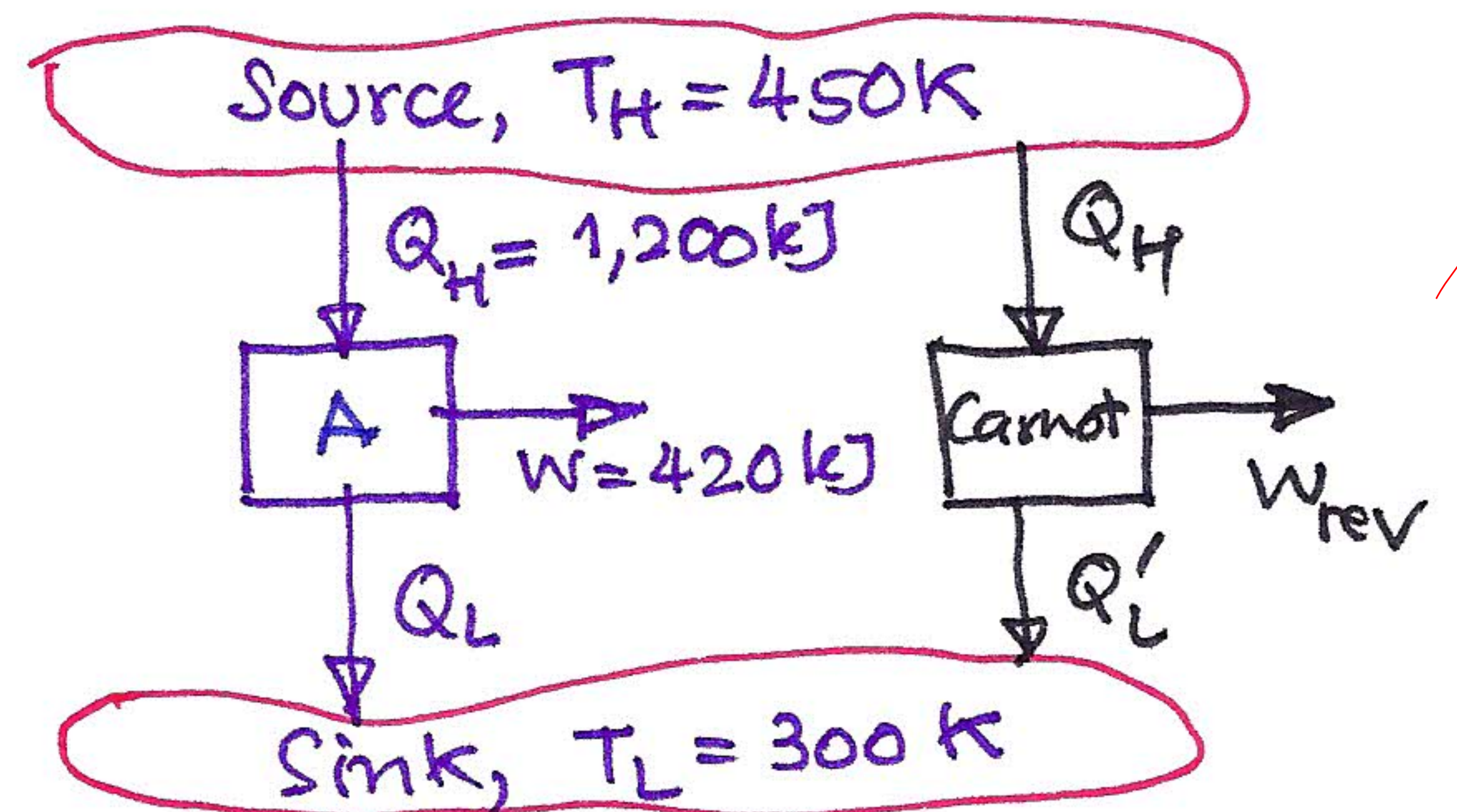


1. An inventor claims to have developed a heat engine that receives 1,200 kJ of heat from a source at 450 K and produces 420 kJ of net work while rejecting the waste heat to a sink at 300 K. Is this a reasonable claim? Why (5 Marks)

System: Heat Engine.

Analysis:

Carnot Principle:  $\eta_{irr} < \eta_{rev}$



Solution:

Consider the claimed engine. (Engine A)

$$\eta_{th} = \frac{W_{net}}{Q_H} \times 100\% = \frac{420 \text{ kJ}}{1,200 \text{ kJ}} \times 100\% = 35.0\%$$

Consider a Carnot Heat Engine operate between the same heat source and heat sink, also receives the same amount of  $Q_H$ .

$$\eta_{rev} = 1 - \frac{T_L}{T_H} = 1 - \frac{300 \text{ K}}{450 \text{ K}} = 0.333 = 33.3\%$$

$\therefore \eta_{irr} > \eta_{rev}$ ; this violate the Carnot principle.

Therefore, this claim is UNREASONABLE (impossible) Ans.



เลขที่สอบ..... Name .....

Examiner: Assoc.Prof.Sommai Priprem, PhD.

2. An air conditioning system is used to maintain a house at a constant temperature of  $25^\circ\text{C}$ . The house is gaining heat from outdoors at a rate of  $45,000\text{ kJ/h}$ , and the heat generated in the house from the people, lights, and appliances amounts to  $6,000\text{ kJ/h}$ . For a COP of 2.5, determine the required power input to this air conditioning system (5 Marks)

System: Air Conditioner

Analysis:  $\dot{W} = \frac{\dot{Q}_L}{\text{COP}}$

Solution:

Consider the house;  
to maintain constant temp.

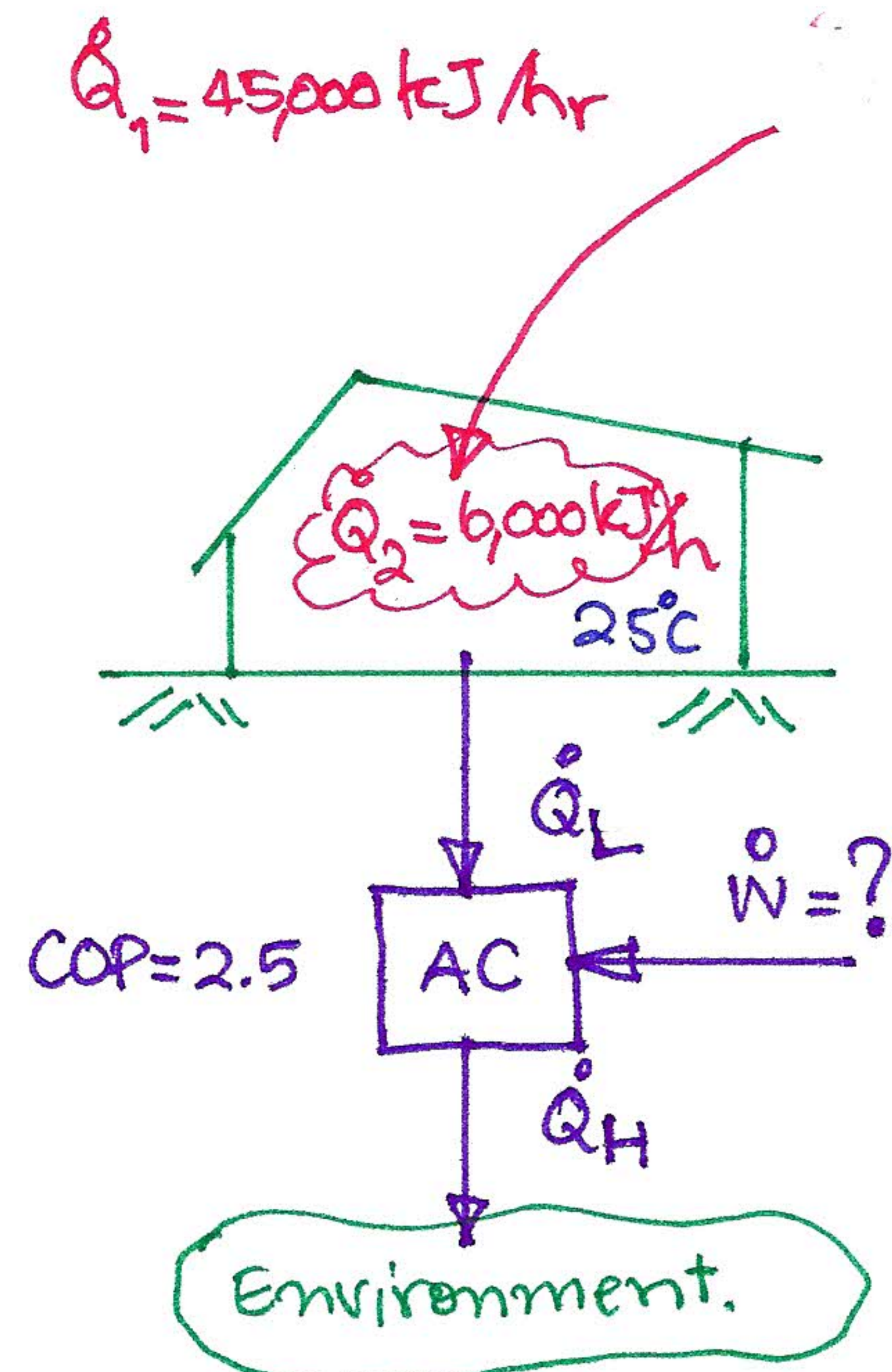
$$\sum \dot{Q}_{\text{in}} = \sum \dot{Q}_{\text{out}}$$

$$\begin{aligned}\sum \dot{Q}_{\text{in}} &= \dot{Q}_1 + \dot{Q}_2 \\ &= (45,000 + 6,000)\text{ kJ/h} \\ &= 51,000\text{ kJ/h} \times \frac{1}{3,600\text{ s/h}}\end{aligned}$$

$$\text{and } \dot{Q}_L = \sum \dot{Q}_{\text{out}} = 14.17\text{ kW}$$

$$\therefore \dot{W} = \frac{\dot{Q}_L}{\text{COP}} = \frac{14.17\text{ kW}}{2.5} = 5.67\text{ kW}$$

The power required is  $5.67\text{ kW}$  Answer

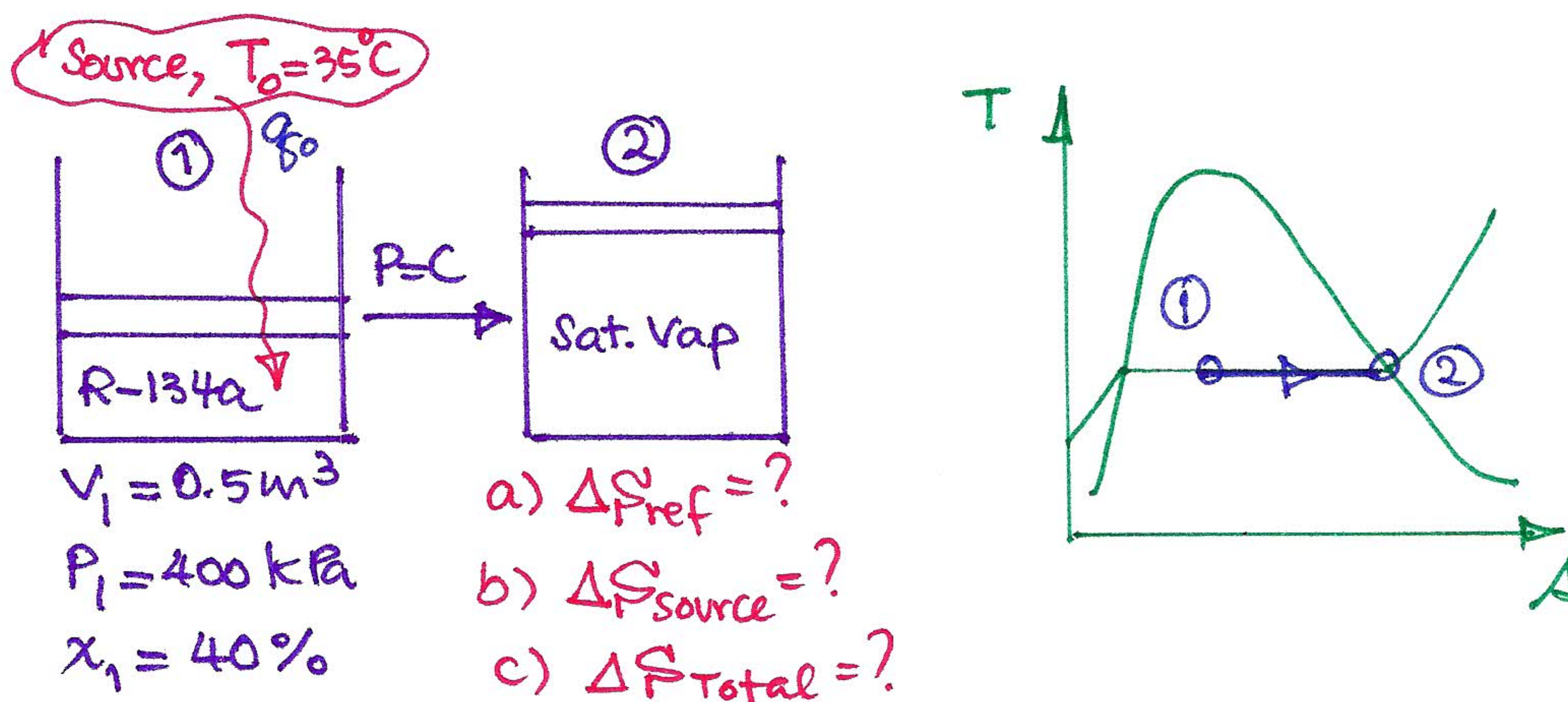




เลขที่สอบ..... Name .....

Examiner: Assoc.Prof.Sommai Priprem, PhD.

3. A piston-cylinder device contains refrigerant-R-134a initially at  $0.5\text{-m}^3$  400 kPa and 40 percent quality. Heat is transferred to the refrigerant from a source at  $35^\circ\text{C}$  until the refrigerant becomes saturated vapour. If the process occurred at constant pressure determine (a) the entropy change of the refrigerant, (b) the entropy change of the heat source, and (c) the total entropy change for this process. (d) does this process violates the principle of increase of entropy, why. (10 marks)



System: R-134a, Closed system.

Solution: state ①  $P_1 = 400\text{ kPa}$ ,  $x_1 = 40\%$ , Table A-15b.

$$v_1 = v_f + x_1 v_{fg} = (0.0008) + 0.4(0.0509 - 0.0008) = 0.0208\text{ m}^3/\text{kg}$$

$$m = \frac{V_1}{v_1} = \frac{0.5\text{ m}^3}{0.0208\text{ m}^3/\text{kg}} = 24\text{ kg}$$

$$h_1 = h_f + x_1 h_{fg} = 62.0 + 0.4(190.32) = 138.13\text{ kJ/kg}$$

$$s_1 = s_f + x_1 s_{fg} = 0.2399 + 0.4(0.6746) = 0.5097\text{ kJ/kgK}$$

state ②  $P_2 = P_1 = 400\text{ kPa}$ , Sat. vapor.

$$h_2 = h_g = 252.32\text{ kJ/kg}; \quad s_2 = s_g = 0.9145\text{ kJ/kgK}$$

$$\text{a) } \Delta S_{\text{ref}} = m(s_2 - s_1) = 24\text{ kg}(0.9145 - 0.5097)\text{ kJ/kgK} = 9.7138\text{ kJ/K} \quad \text{Answer}$$

$$\text{b) } q_0 = -q_2 = w_2 + u_2 - u_1 = P(v_2 - v_1) + u_2 - u_1 = h_2 - h_1$$

$$\Delta S_{\text{source}} = \frac{Q_0}{T_0} = \frac{m q_0}{T_0} = \frac{(24\text{ kg})(138.13 - 252.32)\text{ kJ/kg}}{(35 + 273)\text{ K}} = -9.196\text{ kJ/K}$$

$$\text{c) } \Delta S_{\text{Total}} = \Delta S_{\text{ref}} + \Delta S_{\text{source}} = 9.7138 - 9.1963 = 0.5175\text{ kJ/K}$$

Does not violate Princ. of increase of entropy  $\because \Delta S_{\text{Total}} > 0$  Answer



เลขที่สอบ..... Name .....

Examiner: Assoc.Prof.Sommai Priprem, PhD.

4. Steam enters an adiabatic turbine at 15 MPa and 400°C with a mass flow rate of 3 kg/s and leaves at 10 kPa. The adiabatic efficiency of the turbine is 0.95. Neglecting the kinetic energy change of the steam, determine (a) the temperature at the turbine exit and (b) the power output of the turbine.

System: steam, Turbine

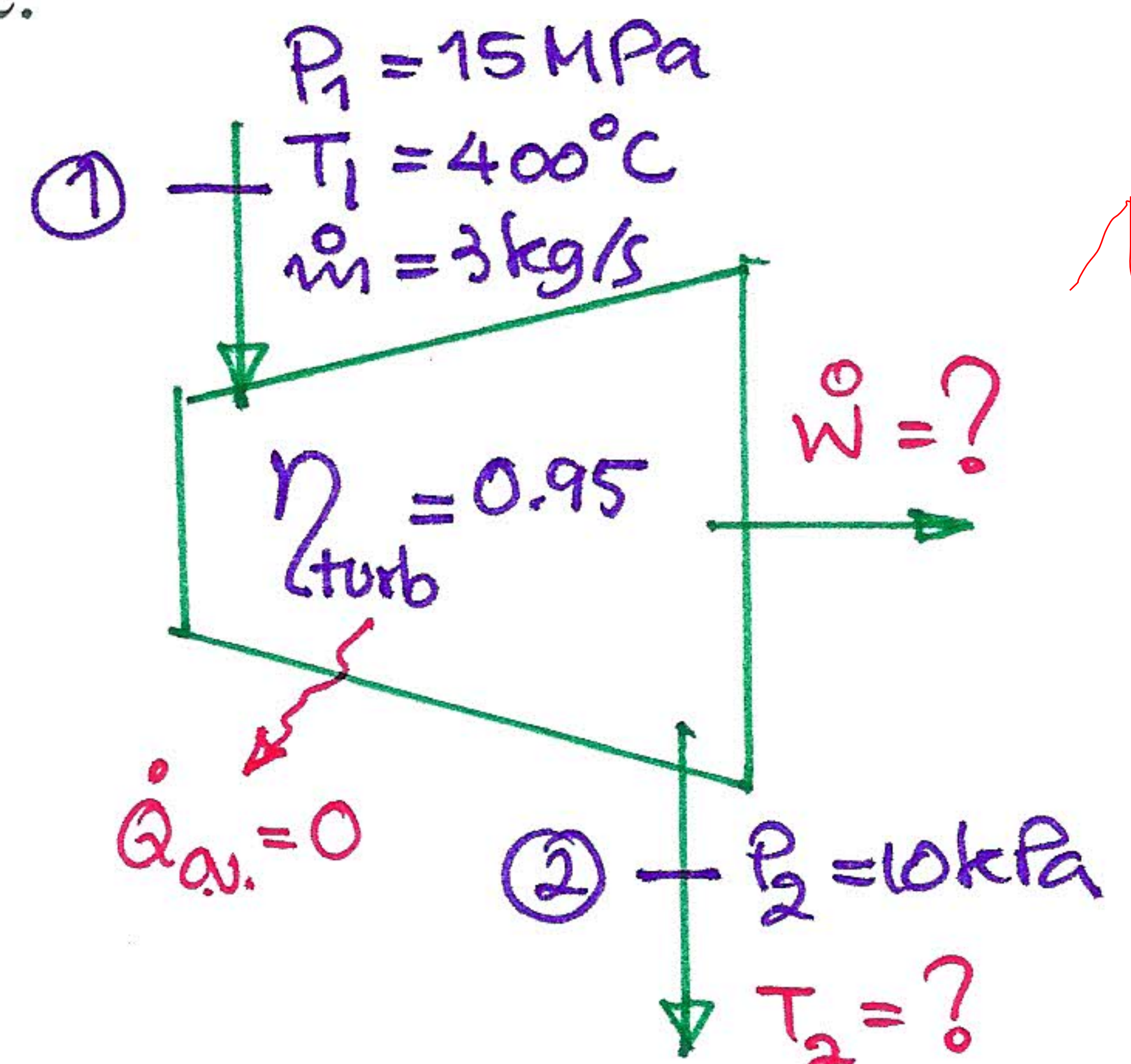
Assumption: SSSF, neglect  $\Delta KE$ ,  $\Delta PE$

Analysis:  $T_2 \rightarrow$  state 2

$$\dot{W} = \dot{m} w$$

$$\eta = \frac{w_a}{w_s}$$

$$w_s = h_1 - h_{2s}$$



Solution state ① 15 MPa, 400°C  $\Rightarrow$  superheated vap.

Table A-6;  $h_1 = 2975.5 \text{ kJ/kg}$ ;  $s_1 = 5.8811 \text{ kJ/kg K}$

Consider isentropic process  $1 \rightarrow 2s$ ;  $s_{2s} = s_1$ ,  $P_2 = 10 \text{ kPa}$ .

$\because s_f < s_{2s} < s_{fg} \Rightarrow$  mixture

$$x_{2s} = \frac{s_{2s} - s_f}{s_{fg}} = \frac{5.8811 - 0.6493}{7.5009} = 0.6975$$

$$h_{2s} = h_f + x_{2s} h_{fg} = (191.8) + (0.6975)(2392.8) = 1860.8 \text{ kJ/kg}$$

$$\text{1st law: } w_s = h_1 - h_{2s} = (2975.5 - 1860.8) = 1114.7 \text{ kJ/kg}$$

$$w_a = \eta w_s = (0.95)(1114.7) \text{ kJ/kg} = 1059.0 \text{ kJ/kg}$$

$$\dot{W} = \dot{m} w_a = \left(3 \frac{\text{kg}}{\text{s}}\right)(1059.0 \text{ kJ/kg}) = 3176.9 \text{ kW} \quad \text{Answer (b)}$$

1st law: actual process,  $w_a = h_1 - h_2 \Rightarrow h_2 = h_1 - w_a$

$$h_2 = (2975.5 - 1059.0) = 1916.5 \text{ kJ/kg}$$

At  $P = 10 \text{ kPa}$ ,  $h_f < h_2 < h_g \Rightarrow$  ② is mixture

$$\therefore T_2 = T_{\text{sat}} \text{ at } 10 \text{ kPa} = 45.81^\circ \text{C} \quad \text{Answer (a)}$$