**Description:**

There are many type of air conditioning system used such as air-cooled split type, air-cooled compact, water-cooled chiller system. The performance of each system is much depended on its type and operation. The type of the system must be selected for specific design usage and operation. However, in many cases, the operation is far different from that of the design values. The performance, therefore, depended on each operation.

This experiment is to measure the performance of the special (non-industrial) configuration of air conditioner which comprised of water-cooled evaporator and air-cooled condenser. The system is assumed to work in air heating mode, so called **heat pump**, and water cooling mode, so called **refrigerator or chiller**. The coefficient of performance (COP) is compared among actual operation and ideal (reversible) theory.

**Objectives:**

1. To measure the performance of air-conditioning system for both heating and cooling modes
2. To evaluate the time to steady state effect
3. To compare the actual coefficient of performance of the apparatus against that of ideal cycle.

**Theory:**

Vapor Compression Refrigeration Cycle

The vapor compression refrigeration cycle is a common method for transferring heat from a low temperature to a high temperature as schematically shown in the following figure.

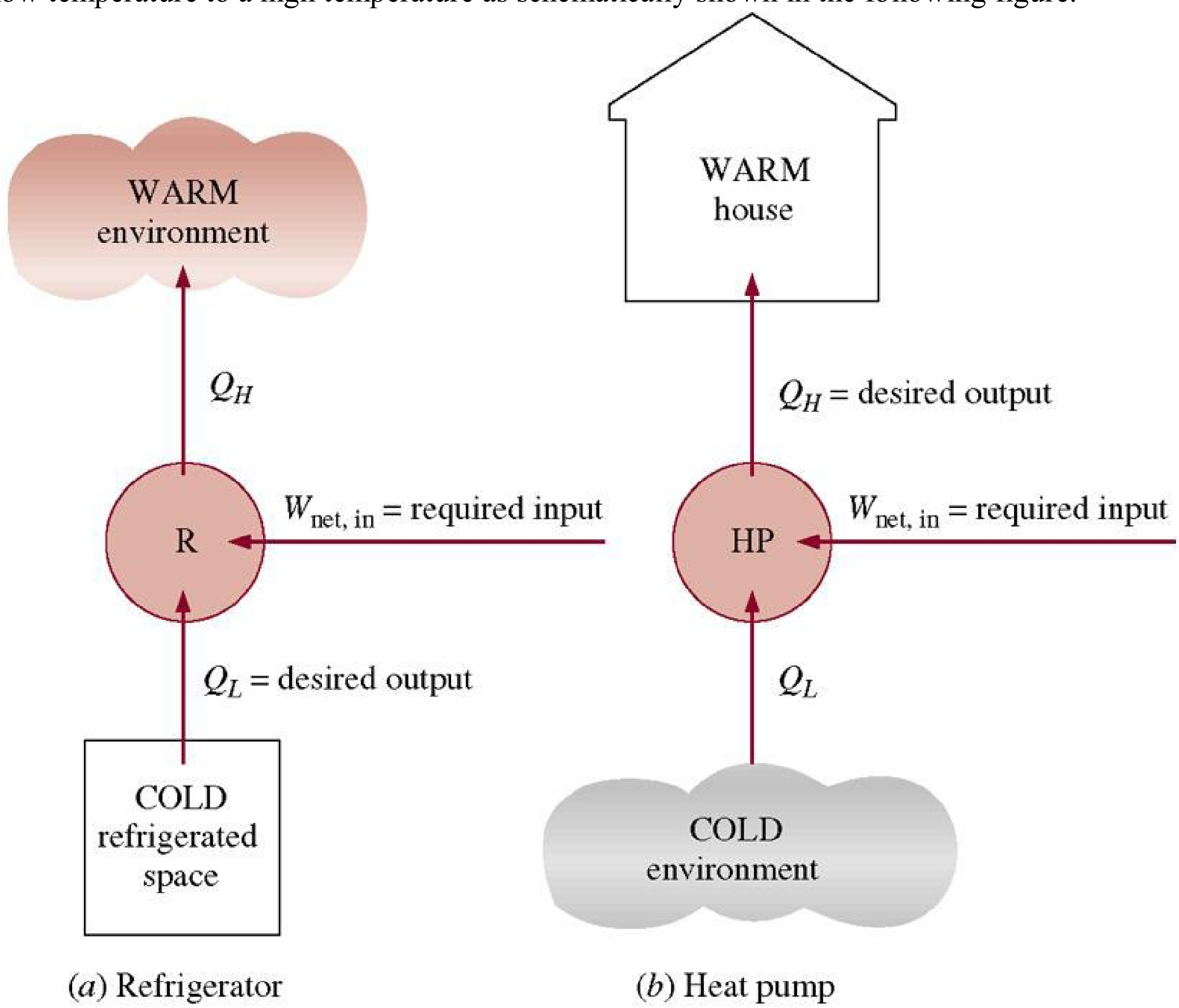



**Figure 1 Schematic of refrigeration cycle**

Coefficient of Performance (COP)

The performance of refrigerators and heat pumps is expressed in term of the coefficient of performance (COP)

$$(COP_R)_{actual} = \frac{\text{Desired output}}{\text{Required input}} = \frac{\text{Cooling effect}}{\text{Work input}} = \frac{Q_L}{W_{\text{net, in}}}$$

$$(\text{COP}_{\text{HP}})_{actual} = \frac{\text{Desired output}}{\text{Required input}} = \frac{\text{Heating effect}}{\text{Work input}} = \frac{Q_H}{W_{\text{net, in}}}$$

$$\text{COP}_{\text{HP}} = \text{COP}_{\text{R}} + 1$$

The reverse Carnot cycle coefficient of performance can be evaluated as

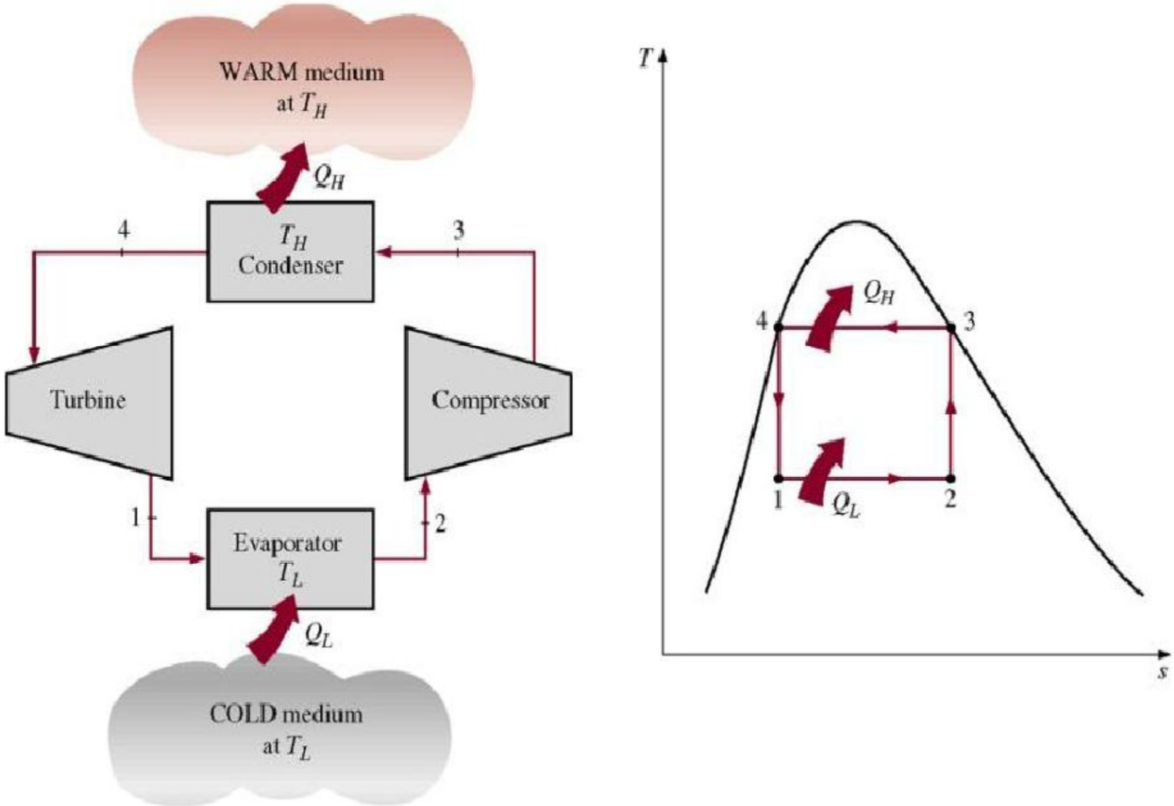



**Figure 2 Reverse Carnot cycle**

If the Carnot device is caused to operate in the reversed cycle, the reversible heat pump is created. The COP of reversible refrigerators and heat pumps are given in a similar manner to that of the Carnot heat engine as

$$(COP_R)_{Carnot} = \frac{Q_L}{Q_H - Q_L} = \frac{1}{\frac{Q_H}{Q_L} - 1}$$

$$= \frac{T_L}{T_H - T_L} = \frac{1}{\frac{T_H}{T_L} - 1}$$

$$(COP_{HP})_{Carnot} = \frac{Q_H}{Q_H - Q_L} = \frac{\frac{Q_H}{Q_L}}{\frac{Q_H}{Q_L} - 1}$$

$$= \frac{T_H}{T_H - T_L} = \frac{\frac{T_H}{T_L}}{\frac{T_H}{T_L} - 1}$$

These are the maximum possible COPs for a refrigerator or a heat pump operating between the
temperature limits of $T_H$ and $T_L$.

The coefficient of performance may be compared with an ideal performance based upon
the temperature difference across the heat pump circuit:-

$$(COP_R)_{\max} = \frac{T_{comp,in}}{T_{comp,out} - T_{comp,in}}$$

$$(COP_{HP})_{\max} = \frac{T_{comp,out}}{T_{comp,out} - T_{comp,in}}$$

**Experimental apparatus:**

Figure 3 shows a general view of the apparatus which is based on the Vesatemp high level Air condition type VH 215. This type of machines are widely used for the air conditioning
of individual rooms but the specific feature of the Versatemp is that it requires a supply of circulating water that may be used either as the source of heat when the machine is acting as a heat pump, or as the sink when air cooling is taking place.


**Figure 3 General view of the experimental apparatus**

In order to simplify the experimental technique, the air conditioner is modified in an important respect when compared with the normal commercial – version : the duplex low speed fan that normally circulates air, through the conditioner is replaced by a single high speed fan delivering air to a small circular duct. The purpose of this modification is to develop a sufficiently high velocity head to ensure that air flow may be measured by a simple pitot tube and manometer, but the greatly increases the level of the conditioner and also results in some reduction is efficiency. This in no way affects the performance, and in particular the noise lever, is interior to that to be expected in normal practice. The fan in the normal unit is inaudible.

The air conditioner is completely self contained and consists of a hermetically sealed refrigeration system driven by a l hp motor, a reversing valve, fan and motor, condensate collector and electrical controls.

The air to be conditioned enters by the finned refrigerant to – air heat exchanger, passes through the centrifugal fan which is driven by a motor immersed in the air flow, and is discharged to a duct of circular cross-section carrying a pitot tube and mercury- in – glass thermometer. When the air in being cooled and the relative humidity is high enough, moisture is deposited or the heat exchanger and drained off to a measuring vessel.

The refrigerant- to water heat exchanger is a co-axial wire wound unit and is thermally insulated externally.

Two separate units are associated with the air conditioner. The first consists of and electrical control panel carrying an isolator and warning light, fuses, the necessary control and change over switches, and wattmeter. It is connected by flexible cable to the air conditioner and to the second independent unit.

The latter carries a flow meter for measurement of the quantity of water passing through the conditioner. Thermometers for water inlet and outlet temperatures, an inclined manometer for use with the pitot-static tube for air flow measurement and a vessel containing a 2 kW immersion heater is sometimes necessary when the conditioner is operating as a heat pump extracting heat from the circulating water since if the temperature of the latter on entry to the conditioner falls below about 10 C. There is a likelihood of freezing taking place. This unit is connected by flexible cable to the control panel.

The following instruments are provided:

a) Watt meter for measurement of electrical power input to refrigerator compressor and to
fan.

b) Thermometers for measurement of air inlet and outlet temperatures both dry bulb and wet
bulb.

c) Thermometers for measurement of cooling water inlet and outlet temperatures both dry
bulb and wet bulb.

d) Pitot-static tube and inclined manometer for measurement of air flow.

e) Cooling water flow meter.

f) Thermocouple at inlet and outlet to refrigerator compressor.

**Calculation:**

The apparatus can be used to evaluate the COP of both as heat pump and as refrigerator by using corresponding thermal output. Referring to

$$(COP_R)_{actual} = \frac{\text{Desired output}}{\text{Required input}} = \frac{\text{Cooling effect}}{\text{Work input}} = \frac{Q_L}{W_{\text{net, in}}}$$

$$(COP_{HP})_{actual} = \frac{\text{Desired output}}{\text{Required input}} = \frac{\text{Heating effect}}{\text{Work input}} = \frac{Q_H}{W_{\text{net, in}}}$$

$$(COP_{HP})_{actual} = (COP_R)_{actual} + 1$$

Cooling effect, $Q_L$

$$Q_L = \dot{m}_{water} C_{p,water} \left( T_{water,in} - T_{water,out} \right)$$

The water mass flow rate (kg/s), $\dot{m}_{water}$ , can be calculate from the measurement of volume flow rate as,

$$\dot{m}_{water} = \rho_{water} \dot{V}_{water}$$

$$= \rho_{water} \left( \frac{51.3 (H_{water})^{0.468}}{1000 \times 3600} \right), \quad \text{kg/s}$$

Where $\dot{V}_{water}$ is volumetric water flow rate

$H_{water}$ is the measured circulating water flow meter head (cm.$H_2O$.)

Heating effect, $Q_H$

$$Q_H = \dot{m}_{air} \left( h_{air,out} - h_{air,in} \right)$$

The air flow through the conditioner is measured by means of a pitot tube mounted in the
center of the discharge duct. The pressure of the air at this point is effectively equal to that of the
atmospheric, $P_a$, that can be obtained at the barometer in the laboratory or at http://weather.kku.ac.th/wx200.txt (hectopascal (hPa), a unit of pressure equivalent to about 1/1000 of 1 atmosphere).
and its density is given by the gas equation:-

$$\left(\frac{P_a}{\rho_{air}}\right) = RT, \qquad \text{where R = 287 J/kg K for air}$$

The velocity $U$, corresponding to a velocity head $H_{air}$ (cm.$H_2O$) as measured by the pitot tube is
given by:-

$$\frac{\rho U^2}{2} = 98.1 H_{air}, \qquad \text{where 1 cm.}H_2O = 98.1 \text{ Pa}$$

That is

$$U = 237.3\sqrt{\frac{H_{air} T_{DB,out}}{P_a}}$$

The mean velocity in the duct may be calculated by traversing the pitot tube across a horizontal
and vertical diameter and integrating to obtain the total flow. Such a calibration for the apparatus
in this experiment gives a value:-

$$\bar{U} = 0.96U$$

Therefore the volumetric flow rate in the duct, diameter D, is given by:-

$$\dot{V}_{air} = \frac{\pi D^2}{4} \times 0.96 \times 237.3\sqrt{\frac{H_{air} T_{DB,out}}{P_a}}$$

for this case, D = 0.073 m, therefore:-

$$\dot{V}_{air} = 0.953\sqrt{\frac{H_{air} T_{DB,out}}{P_a}}$$

By using the gas equation to obtain the air density the air mass flow rate is then given by:-

$$\dot{m}_{air} = 0.00332\sqrt{\frac{H_{air} P_a}{T_{DB,out}}}$$

Where $H_{air}$ = Pitot tube air head, cm.$H_2O$
$P_a$ = atmospheric pressure, Pa
$T_{DB,out}$ = Outlet air temperature, K

The enthalpy of air can be obtained by using either psychometric chart or Engineering Equation Solver (EES). The independent variables are dry bulb temperature $T_{DB}$ and wet bulb temperature, $T_{WB}$, in Kelvin (K).

**Enthalpy of moist air**

Moist air is a mixture of dry air and water vapor. In atmospheric air, water vapor content
varies from 0 to 3% by mass. The enthalpy of moist and humid air includes the

- enthalpy of the dry air - the sensible heat – and
- the enthalpy of the evaporated water - the latent heat

Specific enthalpy – $h_{air}$ - (J/kg) of moist air is defined as the total enthalpy (J) of the dry air and the water vapor mixture - per unit mass (kg, lb) of moist air.

## Specific Enthalpy of Moist Air

Specific enthalpy of moist air can be expressed as:

$$h_{air} = h_a + \omega\, h_w$$

where

$h_{air}$ = specific enthalpy of moist air (kJ/kg

$h_a$ = specific enthalpy of dry air (kJ/kg)

$\omega$ = humidity ratio (kg/kg)

$h_w$ = specific enthalpy of water vapor (kJ/kg)

## Specific Enthalpy of Dry Air - Sensible Heat

Assuming constant pressure conditions the specific enthalpy of dry air can be expressed as:

$$h_a = Cp_a\, T_{air}$$

where

$Cp_a$ = specific heat capacity of air at constant pressure (kJ/kg °C)
= 1.005 (kJ/kg °C)

$T_{air}$ = air temperature (°C)

Note! *that the enthalpy is 0 kJ/kg at 0oC. This is not correct according the definition of enthalpy in the thermodynamics, but for practical purposes in air psychrometrics this assumption is good enough since our interest is the enthalpy difference.*

## Specific Enthalpy of Water Vapor - Latent Heat

Assuming constant pressure conditions the specific enthalpy of water vapor can be expressed as:

$$h_w = Cpw\, T_{air} + h_{we}$$

where

$Cpw$ = specific heat capacity of water vapor at constant pressure (kJ/kg °C)
= 1.887 (kJ/kg °C)

$T_{air}$ = water vapor temperature at dry air temperature (°C)

$h_{we}$ = evaporation heat of water at 0°C (kJ/kg)
= 2501 (kJ/kg)

There for

$$h_{air} = 1.005T_{air} + \omega(1.887T_{air} + 2501)$$

where

$h_{air}$ = enthalpy (kJ/kg)

$\omega$ = air humidity ratio (kg/kg)

$T_{air}$ = dry air temperature (°C)

The humidity ratio of air, x, can be obtained from Engineering Equation Solver, EES using function

*omega=HumRat(AirH2O,T=T_DB_in,B=T_WB_in,P=Pa)*

## Net power input

The power input to the system is measure from compressor and fan using front panel kW meter.

**Test Procedure and Operation Instructions:**

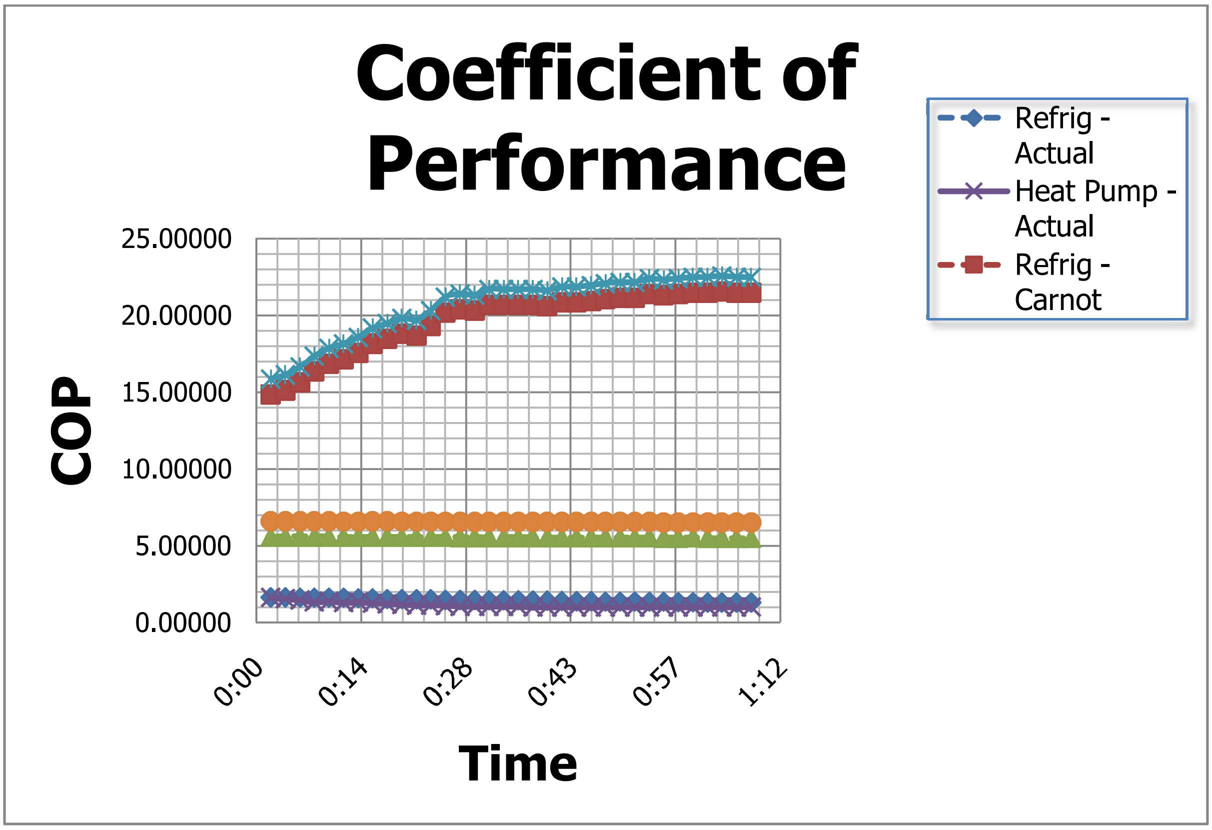

**Figure 4 Main control penel**

1) Make sure that all switches are at OFF position
2) Turn on the cooling water and regulate to give a head, $H_{water}$, of what given by the instructor.
3) Select “AIR CONDITIONER” switch ❷ to “HEAT”
4) Turn the main switch ❶ ON
5) Turn the fan switch ❸ and compressor switch ❹ ON
6) Start recording data using the data collection sheet every 2 minutes until the two successive readings show a change in air and water temperature of not more than 0.3 °C.

**Data analysis and reporting**

1) The calculation of $(COP_R)_{actual}$, $(COP_R)_{carnot}$, and $(COP_R)_{max}$
2) The calculation of $(COP_{HP})_{actual}$, $(COP_{HP})_{carnot}$, and $(COP_{HP})_{max}$
3) Comparison plots of *COP* versus Time

| No. | Time | Air | | | | Water | | | | | Compressor | | Electrical | Barometer | | | | Coefficent of Performance | | | | | |
|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|---|
| | | $T_{DB,in}$ | $T_{WB,in}$ | $T_{DB,out}$ | $H_{air}$ | $T_{water,in}$ | $T_{water,out}$ | Tw,in- Tw,out | m dot,water | $H_{water}$ | $T_{comp,in}$ | $T_{comp,out}$ | $W_{net,in}$ | $P_a$ | $C_p$ | $\rho_{water}$ | $Q_L$ | $COP_R$ | | | $COP_{HP}$ | | |
| | | °C | °C | °C | cm.$H_2O$ | °C | °C | °C | kg/s | cm.$H_2O$ | °C | °C | kW | mm.bar | kJ/kg°C | | | Actual | Carnot | max | Actual | Carnot | max |
| 1 | 0:02 | 28.9 | 25.7 | 52.5 | 2.65 | 26.4 | 15.4 | 11 | 0.0007253 | 15 | 2.8 | 52.1 | 1.4 | 982 | 4.184 | 997 | 0.033381 | 1.66050 | 14.85101 | 5.59736 | 1.65028 | 15.85101 | 6.59736 |
| 2 | 0:04 | 29.3 | 25.8 | 51.4 | 2.65 | 26.4 | 15.4 | 11 | 0.0007253 | 15 | 2.9 | 52.1 | 1.4 | 982 | 4.184 | 997 | 0.033381 | 1.66050 | 15.11825 | 5.61077 | 1.54800 | 16.11825 | 6.61077 |
| 3 | 0:06 | 29.2 | 25.6 | 50.3 | 2.65 | 26.4 | 15.5 | 10.9 | 0.00071871 | 15 | 2.9 | 52.1 | 1.4 | 982 | 4.184 | 997 | 0.032777 | 1.64537 | 15.64362 | 5.61077 | 1.47963 | 16.64362 | 6.61077 |
| 4 | 0:08 | 29.2 | 25.8 | 48.7 | 2.55 | 26.4 | 15.5 | 10.9 | 0.00071871 | 15 | 2.9 | 52.1 | 1.4 | 982 | 4.184 | 997 | 0.032777 | 1.64537 | 16.33889 | 5.61077 | 1.34558 | 17.33889 | 6.61077 |
| 5 | 0:10 | 28.4 | 25.9 | 48.4 | 2.55 | 26.4 | 15.5 | 10.9 | 0.00071871 | 15 | 2.9 | 52.1 | 1.4 | 982 | 4.184 | 997 | 0.032777 | 1.64537 | 16.85387 | 5.61077 | 1.38207 | 17.85387 | 6.61077 |
| 6 | 0:12 | 28.6 | 25.7 | 47.6 | 2.55 | 26.4 | 15.5 | 10.9 | 0.00071871 | 15 | 2.9 | 52.4 | 1.4 | 982 | 4.184 | 997 | 0.032777 | 1.64537 | 17.14869 | 5.57677 | 1.31354 | 18.14869 | 6.57677 |
| 7 | 0:14 | 28.2 | 25.6 | 47.6 | 2.55 | 26.5 | 15.8 | 10.7 | 0.00070677 | 15 | 2.9 | 52.4 | 1.4 | 982 | 4.184 | 997 | 0.031641 | 1.61506 | 17.57015 | 5.57677 | 1.34120 | 18.57015 | 6.57677 |
| 8 | 0:16 | 28.2 | 25.8 | 46.5 | 2.55 | 26.5 | 15.8 | 10.7 | 0.00070677 | 15 | 3 | 52.4 | 1.4 | 982 | 4.184 | 997 | 0.031641 | 1.61506 | 18.16667 | 5.59008 | 1.26814 | 19.16667 | 6.59008 |
| 9 | 0:18 | 28.4 | 25.8 | 46.2 | 2.55 | 26.5 | 16.2 | 10.3 | 0.00068035 | 15 | 3 | 52.4 | 1.4 | 982 | 4.184 | 997 | 0.02932 | 1.55457 | 18.46395 | 5.59008 | 1.23387 | 19.46395 | 6.59008 |
| 10 | 0:20 | 28.5 | 25.8 | 45.5 | 2.55 | 26.5 | 16.2 | 10.3 | 0.00068035 | 15 | 3 | 52.5 | 1.4 | 982 | 4.184 | 997 | 0.02932 | 1.55457 | 18.81789 | 5.57879 | 1.17962 | 19.81789 | 6.57879 |
| 11 | 0:22 | 28.9 | 25.9 | 45.4 | 2.55 | 26.5 | 16.3 | 10.2 | 0.00067374 | 15 | 3 | 52.5 | 1.4 | 982 | 4.184 | 997 | 0.028753 | 1.53945 | 18.70159 | 5.57879 | 1.14510 | 19.70159 | 6.57879 |
| 12 | 0:24 | 28.5 | 25.8 | 44.8 | 2.55 | 26.5 | 16.3 | 10.2 | 0.00067374 | 15 | 3.1 | 52.6 | 1.4 | 982 | 4.184 | 997 | 0.028753 | 1.53945 | 19.31475 | 5.58081 | 1.13229 | 20.31475 | 6.58081 |
| 13 | 0:26 | 28.1 | 25.8 | 44.2 | 2.55 | 26.5 | 16.6 | 9.9 | 0.00065393 | 15 | 3.1 | 52.6 | 1.4 | 982 | 4.184 | 997 | 0.027087 | 1.49409 | 20.18493 | 5.58081 | 1.11982 | 21.18493 | 6.58081 |
| 14 | 0:28 | 28.3 | 25.7 | 43.7 | 2.55 | 26.5 | 16.6 | 9.9 | 0.00065393 | 15 | 3.1 | 52.7 | 1.4 | 982 | 4.184 | 997 | 0.027087 | 1.49409 | 20.39446 | 5.56956 | 1.07145 | 21.39446 | 6.56956 |
| 15 | 0:30 | 28.4 | 25.8 | 43.7 | 2.55 | 26.5 | 16.6 | 9.9 | 0.00065393 | 15 | 3.1 | 52.7 | 1.4 | 982 | 4.184 | 997 | 0.027087 | 1.49409 | 20.32414 | 5.56956 | 1.06475 | 21.32414 | 6.56956 |
| 16 | 0:32 | 28.2 | 25.6 | 43.5 | 2.55 | 26.5 | 16.7 | 9.8 | 0.00064732 | 15 | 3.1 | 52.8 | 1.4 | 981 | 4.184 | 997 | 0.026542 | 1.47897 | 20.68421 | 5.55835 | 1.06408 | 21.68421 | 6.55835 |
| 17 | 0:34 | 28.4 | 25.7 | 43.5 | 2.55 | 26.6 | 16.8 | 9.8 | 0.00064846 | 15 | 3.1 | 52.8 | 1.4 | 981 | 4.184 | 997 | 0.026589 | 1.47891 | 20.69123 | 5.55835 | 1.05034 | 21.69123 | 6.55835 |
| 18 | 0:36 | 28.4 | 25.6 | 43.5 | 2.55 | 26.6 | 16.8 | 9.8 | 0.00064846 | 15 | 3.2 | 52.8 | 1.4 | 981 | 4.184 | 997 | 0.026589 | 1.47891 | 20.69123 | 5.57157 | 1.05000 | 21.69123 | 6.57157 |
| 19 | 0:38 | 28.6 | 25.7 | 43.4 | 2.55 | 26.6 | 16.9 | 9.7 | 0.00064185 | 15 | 3.2 | 52.9 | 1.4 | 981 | 4.184 | 997 | 0.026049 | 1.46380 | 20.69474 | 5.56036 | 1.02946 | 21.69474 | 6.56036 |
| 20 | 0:40 | 28.7 | 25.9 | 43.4 | 2.55 | 26.6 | 16.9 | 9.7 | 0.00064185 | 15 | 3.2 | 52.9 | 1.4 | 981 | 4.184 | 997 | 0.026049 | 1.46380 | 20.62238 | 5.56036 | 1.02308 | 21.62238 | 6.56036 |
| 21 | 0:42 | 28.6 | 25.7 | 43.4 | 2.55 | 26.6 | 17.1 | 9.5 | 0.00062861 | 15 | 3.2 | 53 | 1.4 | 981 | 4.184 | 997 | 0.024986 | 1.43356 | 20.84806 | 5.54920 | 1.02946 | 21.84806 | 6.54920 |
| 22 | 0:44 | 28.7 | 25.8 | 43.4 | 2.55 | 26.6 | 17.2 | 9.4 | 0.000622 | 15 | 3.2 | 53 | 1.4 | 981 | 4.184 | 997 | 0.024463 | 1.41845 | 20.85159 | 5.54920 | 1.02275 | 21.85159 | 6.54920 |
| 23 | 0:46 | 28.6 | 25.6 | 43.4 | 2.55 | 26.6 | 17.2 | 9.4 | 0.000622 | 15 | 3.3 | 53 | 1.4 | 981 | 4.184 | 997 | 0.024463 | 1.41845 | 20.92553 | 5.56237 | 1.02913 | 21.92553 | 6.56237 |
| 24 | 0:48 | 28.7 | 25.8 | 43.3 | 2.55 | 26.6 | 17.4 | 9.2 | 0.00060876 | 15 | 3.3 | 53.1 | 1.4 | 982 | 4.184 | 997 | 0.023433 | 1.38821 | 21.08214 | 5.55120 | 1.01643 | 22.08214 | 6.55120 |
| 25 | 0:50 | 28.6 | 25.7 | 43.3 | 2.55 | 26.6 | 17.4 | 9.2 | 0.00060876 | 15 | 3.3 | 53.1 | 1.4 | 982 | 4.184 | 997 | 0.023433 | 1.38821 | 21.15771 | 5.55120 | 1.02315 | 22.15771 | 6.55120 |
| 26 | 0:52 | 28.7 | 25.7 | 43.3 | 2.55 | 26.7 | 17.4 | 9.3 | 0.00061646 | 15 | 3.4 | 53.2 | 1.4 | 982 | 4.184 | 997 | 0.023987 | 1.40328 | 21.16129 | 5.55321 | 1.01611 | 22.16129 | 6.55321 |
| 27 | 0:54 | 28.5 | 25.8 | 43.3 | 2.55 | 26.7 | 17.5 | 9.2 | 0.00060983 | 15 | 3.4 | 53.2 | 1.4 | 982 | 4.184 | 997 | 0.023474 | 1.38816 | 21.39493 | 5.55321 | 1.03052 | 22.39493 | 6.55321 |
| 28 | 0:56 | 28.6 | 25.8 | 43.3 | 2.55 | 26.7 | 17.5 | 9.2 | 0.00060983 | 15 | 3.4 | 53.4 | 1.4 | 982 | 4.184 | 997 | 0.023474 | 1.38816 | 21.31769 | 5.53100 | 1.02348 | 22.31769 | 6.53100 |
| 29 | 0:58 | 28.7 | 25.9 | 43.3 | 2.55 | 26.7 | 17.7 | 9 | 0.00059657 | 15 | 3.4 | 53.4 | 1.4 | 982 | 4.184 | 997 | 0.022465 | 1.35793 | 21.40217 | 5.53100 | 1.01676 | 22.40217 | 6.53100 |
| 30 | 1:00 | 28.6 | 25.9 | 43.3 | 2.55 | 26.7 | 17.7 | 9 | 0.00059657 | 15 | 3.5 | 53.4 | 1.4 | 982 | 4.184 | 997 | 0.022465 | 1.35793 | 21.48000 | 5.54409 | 1.02381 | 22.48000 | 6.54409 |
| 31 | 1:02 | 28.7 | 26.1 | 43.3 | 2.55 | 26.7 | 17.8 | 8.9 | 0.00058995 | 15 | 3.5 | 53.6 | 1.4 | 982 | 4.184 | 997 | 0.021968 | 1.34282 | 21.48364 | 5.52196 | 1.01742 | 22.48364 | 6.52196 |
| 32 | 1:04 | 28.6 | 26.1 | 43.3 | 2.55 | 26.7 | 17.8 | 8.9 | 0.00058995 | 15 | 3.5 | 53.6 | 1.4 | 982 | 4.184 | 997 | 0.021968 | 1.34282 | 21.56204 | 5.52196 | 1.02447 | 22.56204 | 6.52196 |
| 33 | 1:06 | 28.7 | 26.1 | 43.3 | 2.55 | 26.7 | 17.8 | 8.9 | 0.00058995 | 15 | 3.6 | 53.8 | 1.4 | 982 | 4.184 | 997 | 0.021968 | 1.34282 | 21.48364 | 5.51295 | 1.01742 | 22.48364 | 6.51295 |
| 34 | 1:08 | 28.7 | 26.3 | 43.3 | 2.55 | 26.7 | 17.8 | 8.9 | 0.00058995 | 15 | 3.6 | 53.8 | 1.4 | 982 | 4.184 | 997 | 0.021968 | 1.34282 | 21.48364 | 5.51295 | 1.01809 | 22.48364 | 6.51295 |
| | Average | 28.6 | 25.802941 | 45.008824 | 2.5588235 | 26.561765 | 16.723529 | 9.838235294 | 0.00065056 | 15 | 3.1764706 | 52.838235 | 1.4 | 981.7647059 | 4.184 | 997 | 0.026909 | 1.48473 | 19.67384 | 5.56432 | 1.14122 | 20.67384 | 6.56432 |




**สรุปและวิจารณ์ผลการทดลอง**

จากผลการทดลองเมื่อนำค่าต่างๆมาคำนวณทำให้ได้ค่า $COP_R$ และค่า $COP_{HP}$ ซึ่งเมื่อนำค่ามาเปรียบเทียบกันปรากฏว่าค่าดังกล่าวแตกต่างกันมาก ซึ่งตัวแปรที่ทำให้ค่าทั้งสองแตกต่างกันคือ $T_1$และ $T_2$ ซึ่งถ้าหากอุณหภูมิที่ทางออกและทางเข้าของคอนเดนเซอร์มากจะทำให้ค่ามีค่ามากตามไปด้วย

ในการหาค่าสัมประสิทธิ์สมรรถนะภายในระบบปั๊มความร้อนถ้าต้องการให้ค่าสัมประสิทธิ์สมรรถนะภายในระบบปั๊มความร้อนมีค่าสูงต้องเลือกใช้คอมเพรสเซอร์ที่ดีในขณะอัดสารทำงานและมีการเปลี่ยนแปลงของอุณหภูมิที่น้อยที่สุดเท่าที่จะทำได้จึงจะได้ค่าสัมประสิทธิ์สมรรถนะภายในระบบตามที่ต้องการ

จากการทดลอง ก่อนที่จะทำการอ่านค่าต่างๆ เราจะต้องแน่ใจว่า ระบบอยู่ในสภาวะ SSSF โดยสังเกตจากการใช้เครื่องหล่อเย็นขาออกมีค่าคงที่ ซึ่งจะมีผลทำให้การทดลองวัดค่าต่างๆแม่นยำขึ้น ซึ่งมีผลกับการคำนวณประสิทธิภาพของ Heat pump